

Understanding Process Dynamics: the route to continuous improvement

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Understanding Process Dynamics: the route to continuous improvement

- **Introduction: the languages we speak**
- **Chemistry**
- **Engineering**
- **Batch processing**
- **Continuous processing**
- **Steady state vs controlled state**
- **Perturbations vs Deviations**
- **Regulatory impact of continuous improvement**

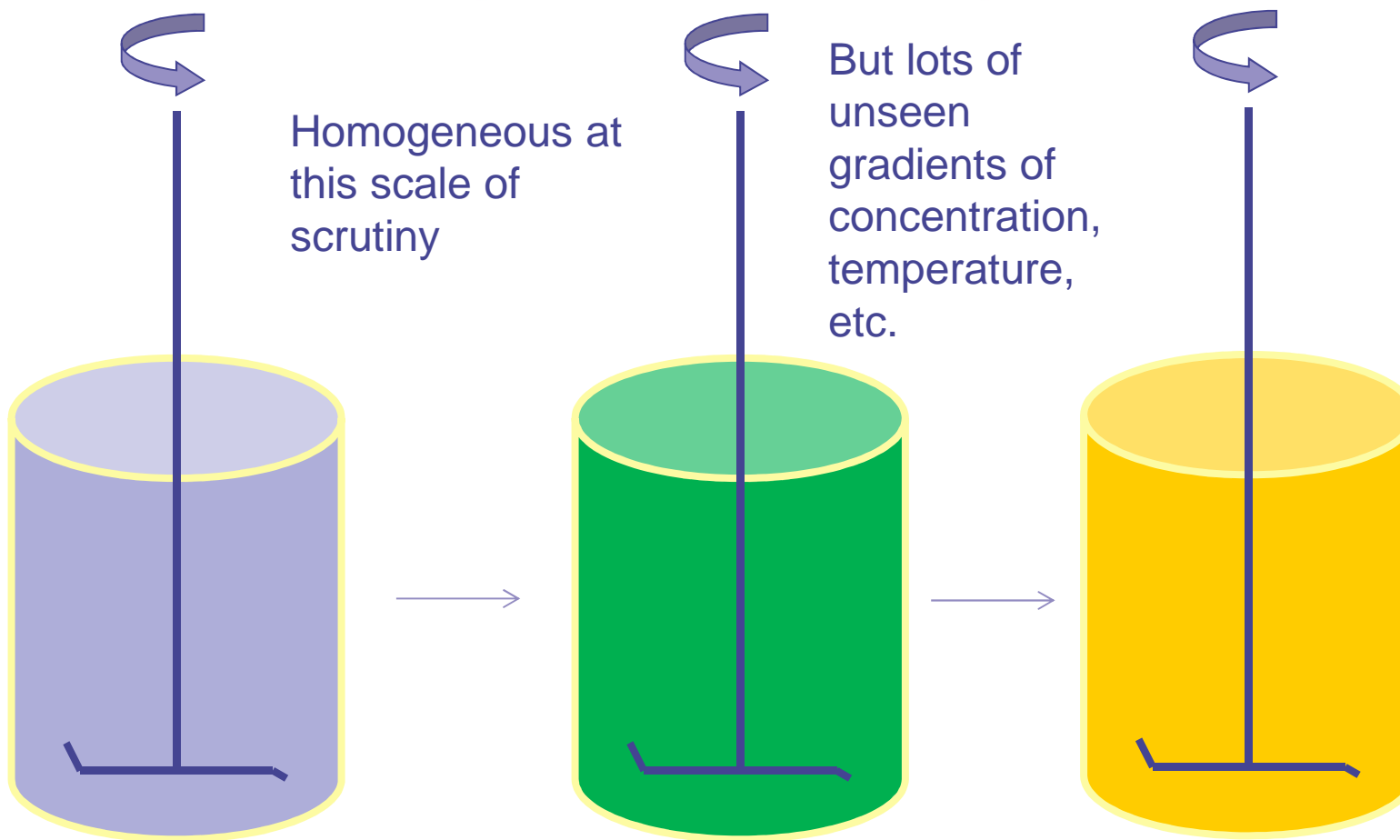
How to translate between related languages

- **Process dynamics for the chemist:**
 - Kinetic measurements – precise, empirical,
 - Equilibrium constants – empirical
 - Strict demarcation between kinetics and thermodynamics
 - Scale of scrutiny generally small
 - Chemists like reactions that proceed to completion
 - Chemists almost always start with a round bottomed flask
- **Process dynamics for the engineer**
 - Mass transfer vs heat transfer
 - Descriptors often not precise
 - Reynold's Number (or other dimensionless numbers) large or small
 - Engineers generally look at whole systems
 - Chemical engineers outside pharmaceutical industry like continuous processes
- **Both approaches are needed**
- **Neither group traditionally strong in statistics, especially Bayesian**
- **Further translations for regulatory submissions and inspections needed!**

Batch processing

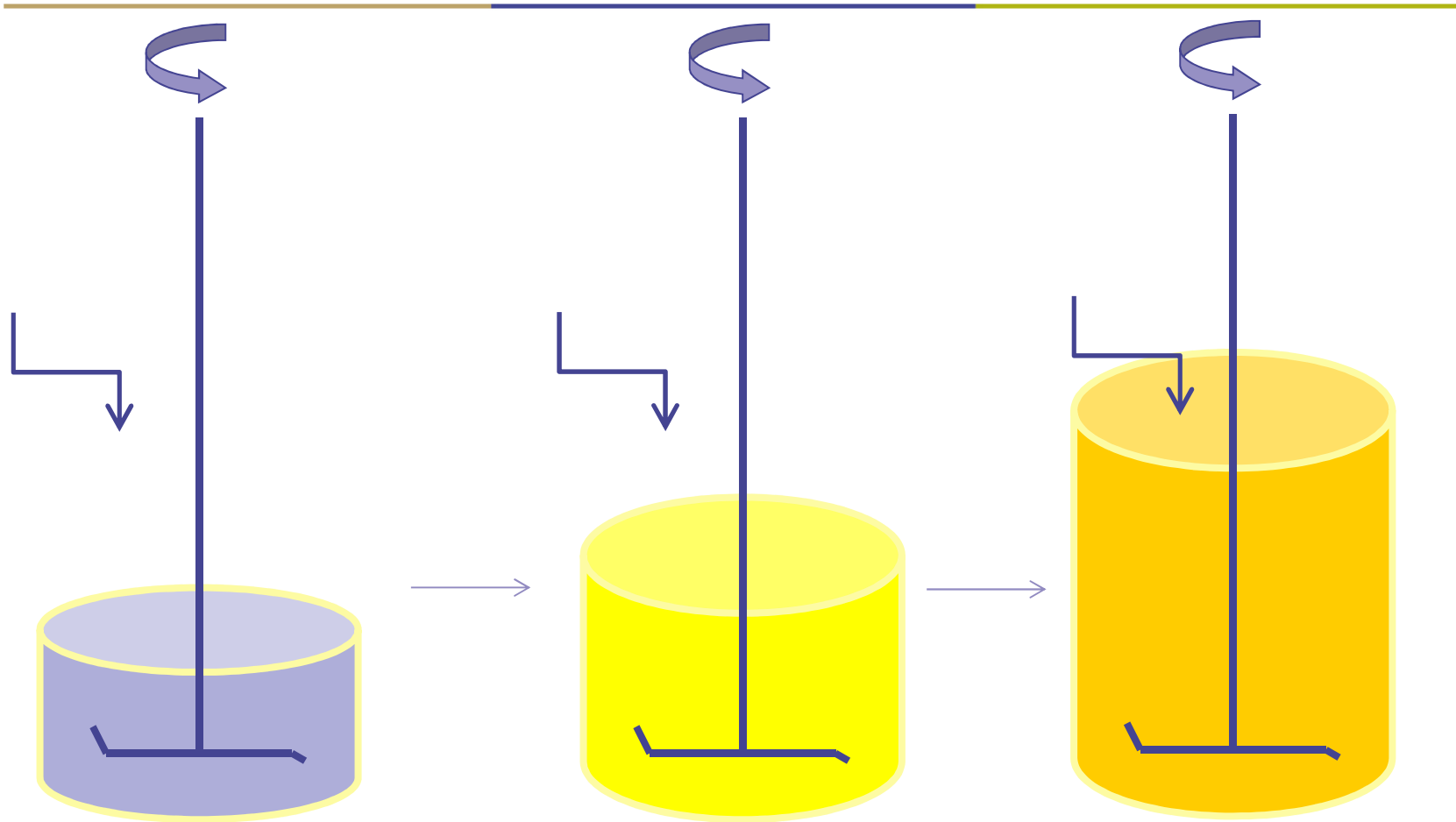
- **Has been the preferred *modus operandum* for pharma industry for decades**
- **API**
 - Use of glass lined or 316 SS/Hastelloy stirred tanks with 3 blade retreat curve impellers or anchor stirrers for reactions
 - Larger stirred tanks for extractions
 - Dedicated crystallisation vessels
 - Basket centrifuge or Nutsche filters for solid isolation
 - General purpose dryer (or filter dryer)
 - Milling
- **DP (oral solid dose)**
 - Blending
 - Wet granulation
 - Drying
 - Blending?
 - Tablet compression (or capsule filling)
 - Tablet coating
 - Printing
 - Packaging

Batch Reaction



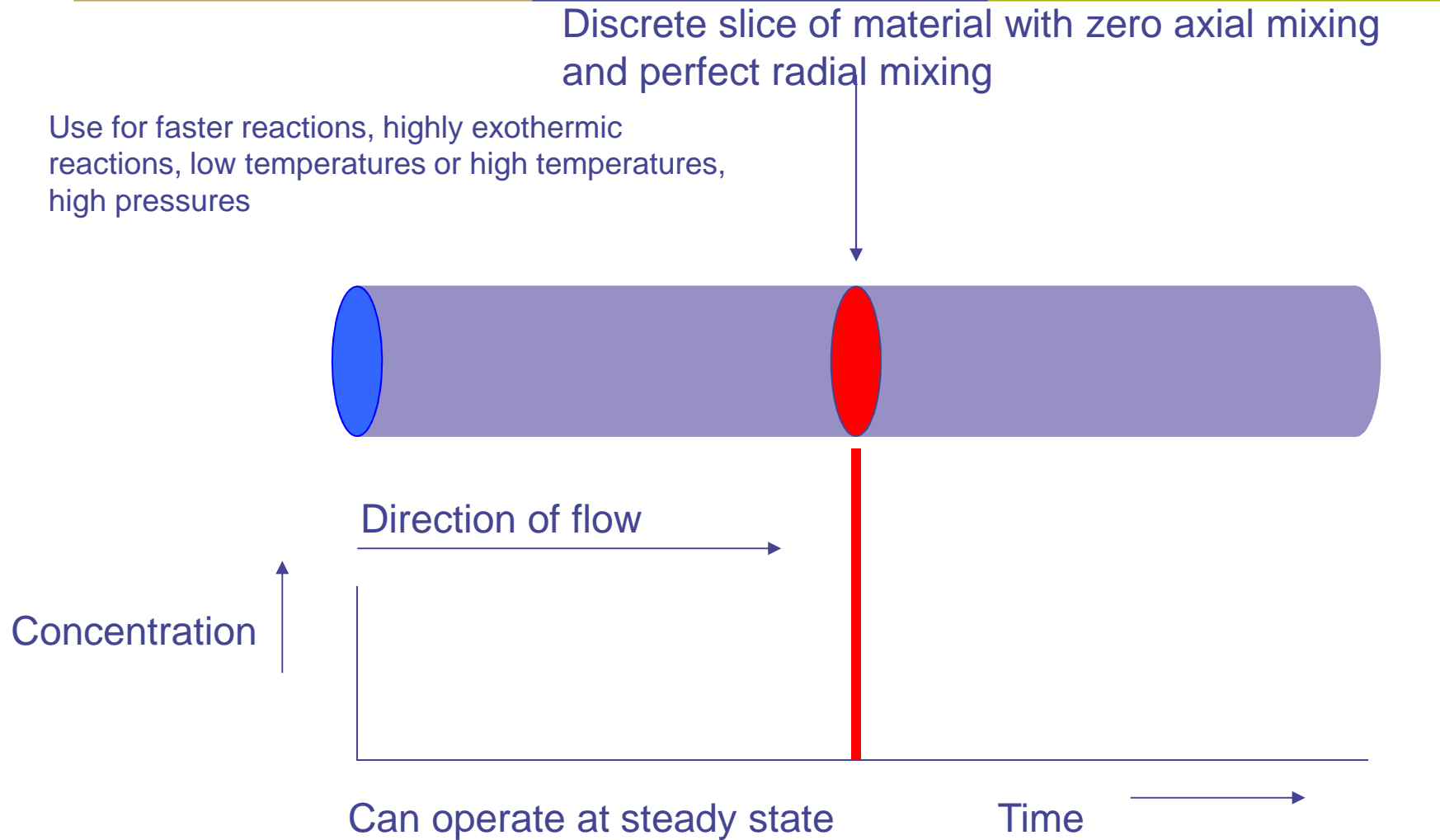
Does not operate at steady state

Semi-batch (fed batch for biotech) processing

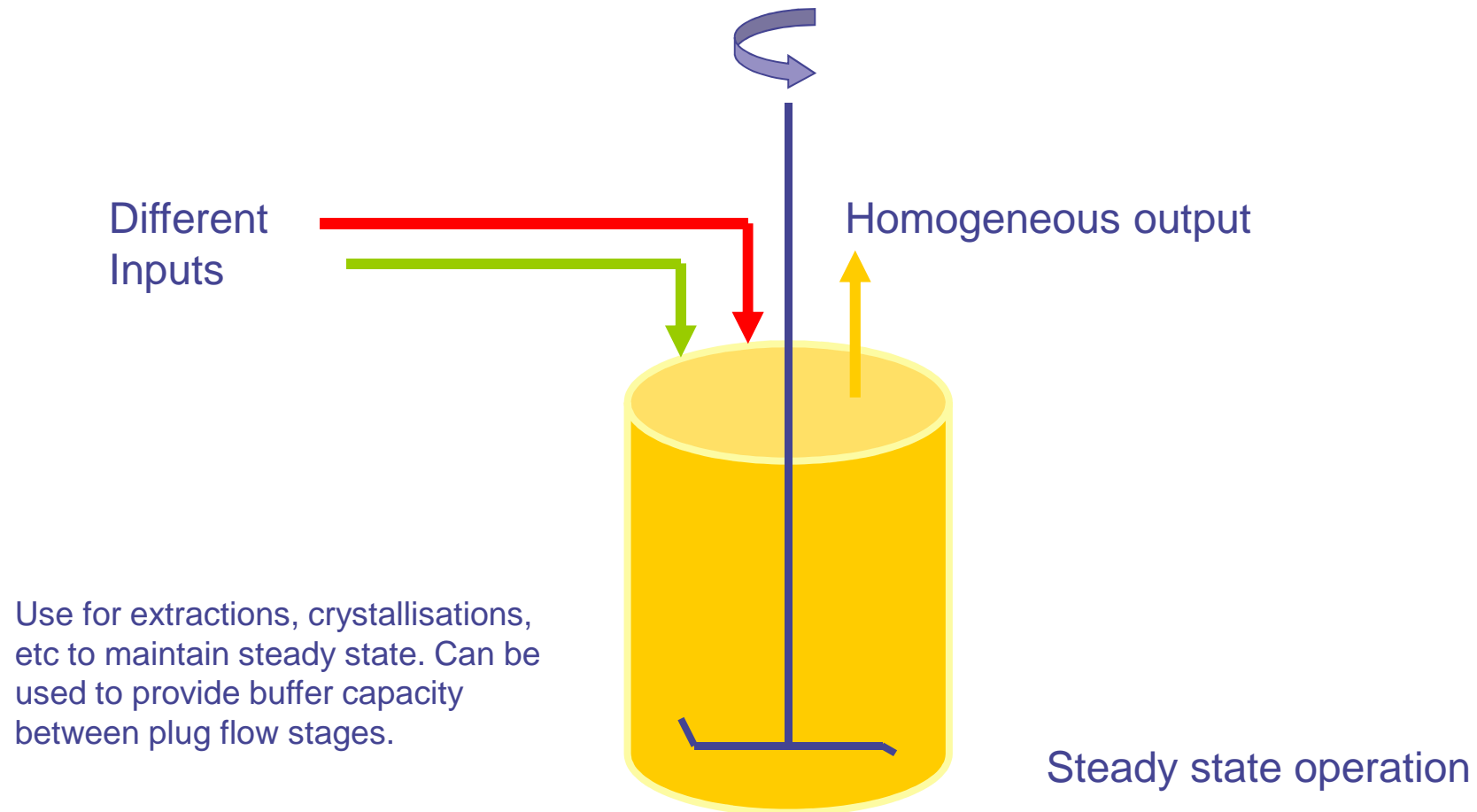


Does not operate at steady state

Idealised plug flow



Idealised CSTR (perfusion for biotech) regime



Flow regime characteristics

● Plug flow

- Used for fast reactions, *etc.*
Kinetic control predominates.
- Highly dynamic and responsive to change
- Susceptible to process “spikes”
- Needs PAT that is fast

● CSTR behaviour

- Equilibrium (thermodynamic) control
- High buffering capacity and slow response time
- Insensitive to process “spikes”
- PAT needs to be stable

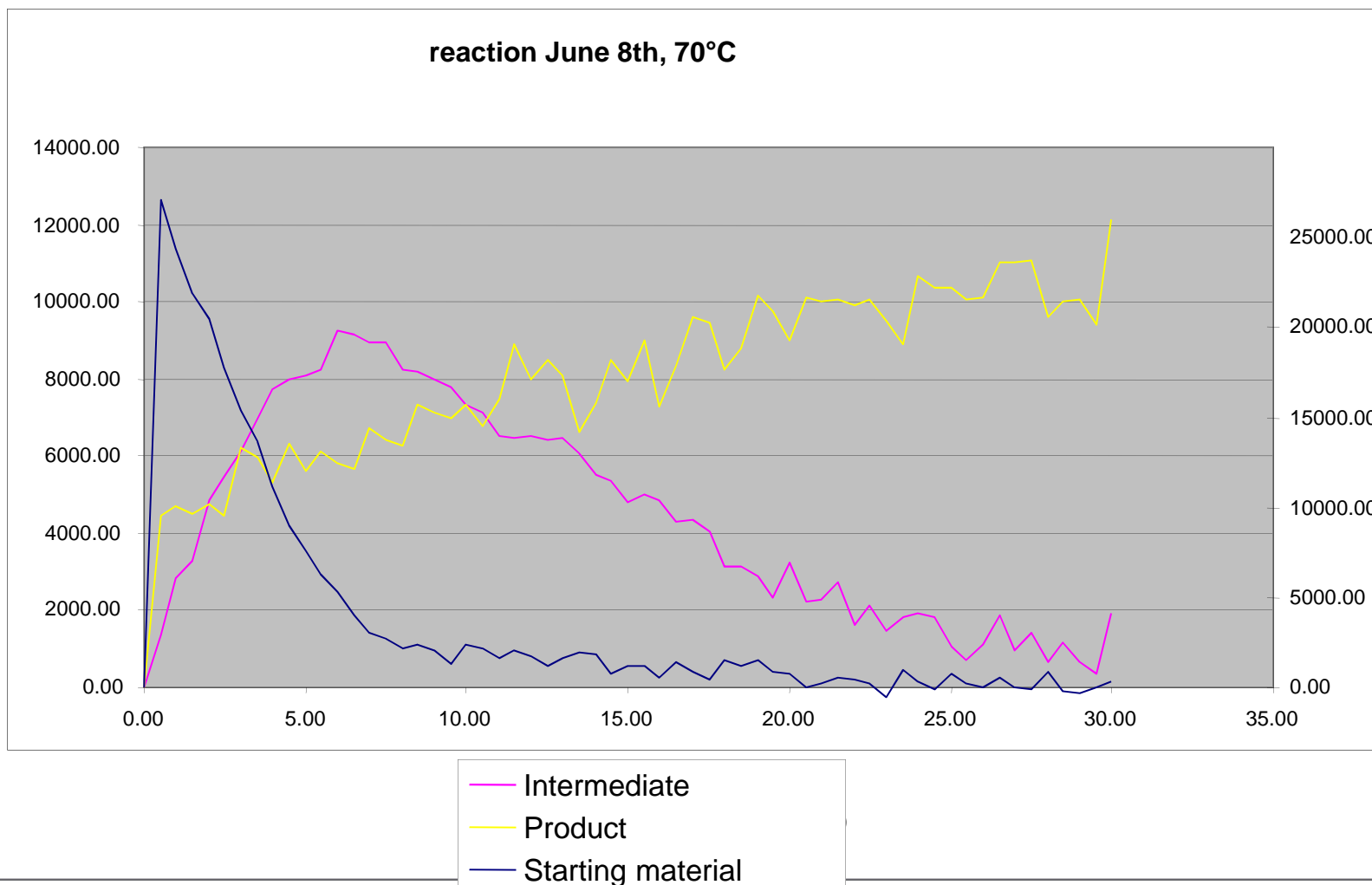
System dynamics and measurements

- **Which regime requires rapid measurement and response?**
 - **Dynamic systems**
 - Plug flow
 - Semi-batch
- **Which regime needs accurate, but possibly imprecise measurement?**
 - **Less dynamic systems**
 - CSTR
- **Which regime can use less accurate, but precise measurement?**
 - **Systems which need batch to batch variation managed**
 - Batch processes

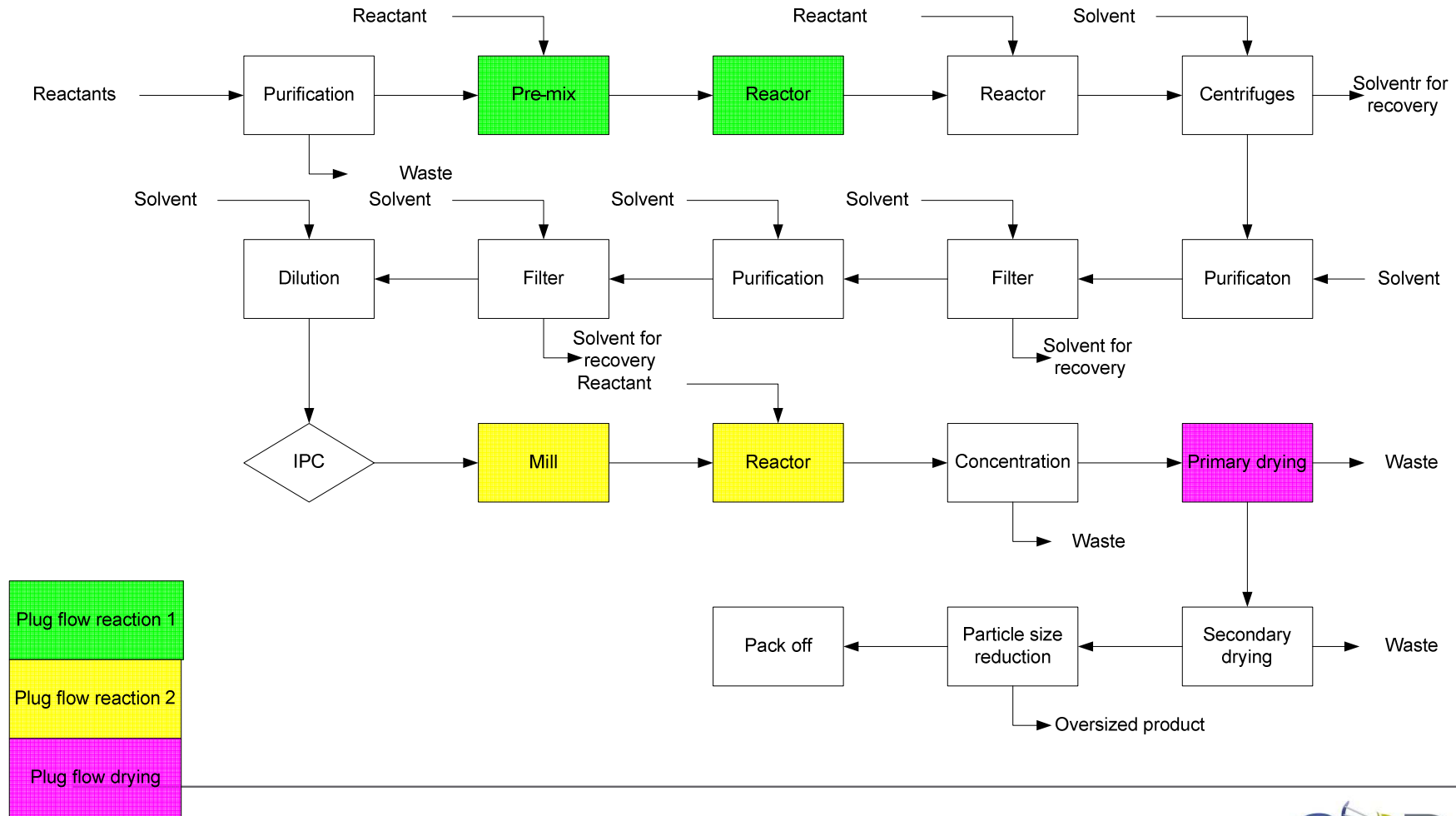
What do you do with process measurements?

- Do you make decisions based upon them?
- Do you make nice graphs?
- Are they made to tell you that everything is as it was before?
- Are they used for predictive maintenance?
- Do they add to process understanding?
- Are they used for continuous improvement?
- Are they made because you filed them?
- Do you believe them?
- How do they serve your business?

Process understanding is needed



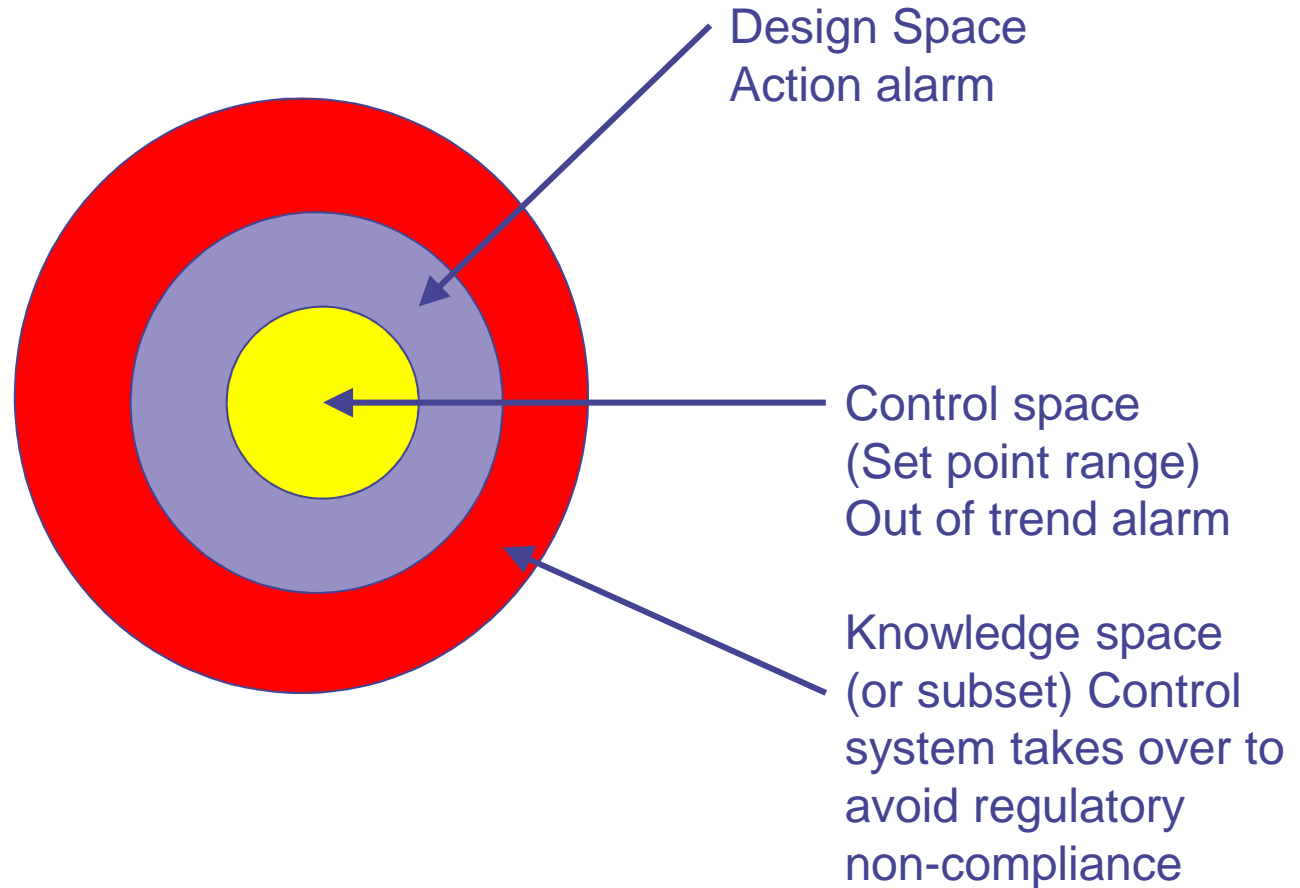
Manufacturing Process Flow – real example operated at multi hundred TPA



Design space and alerts/alarms

Current thinking has moved from maintaining steady state to maintaining control state.

You would like to be able to drive your car at different speeds wouldn't you?



Managing deviations

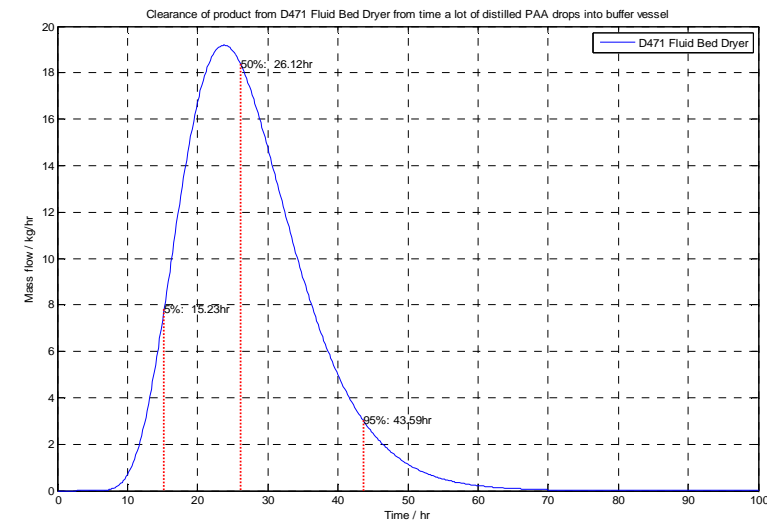
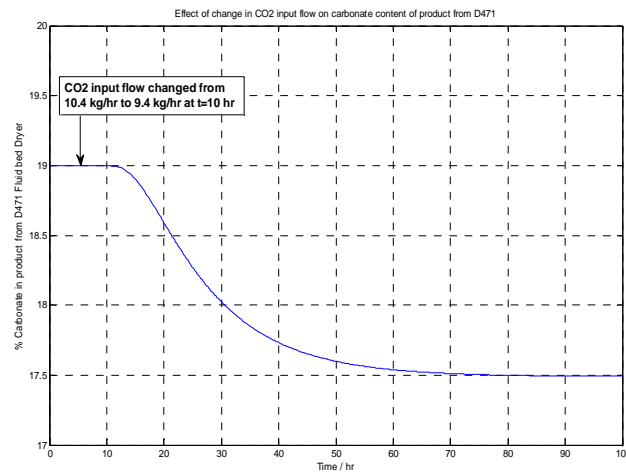
- **Perform risk assessment on unit operations**
 - **Without necessarily considering the reason for a deviation consider what should happen to the product affected**
 - Stop
 - Keep going
 - Divert affected product to waste
 - **Do this during design phase!**

Deviations

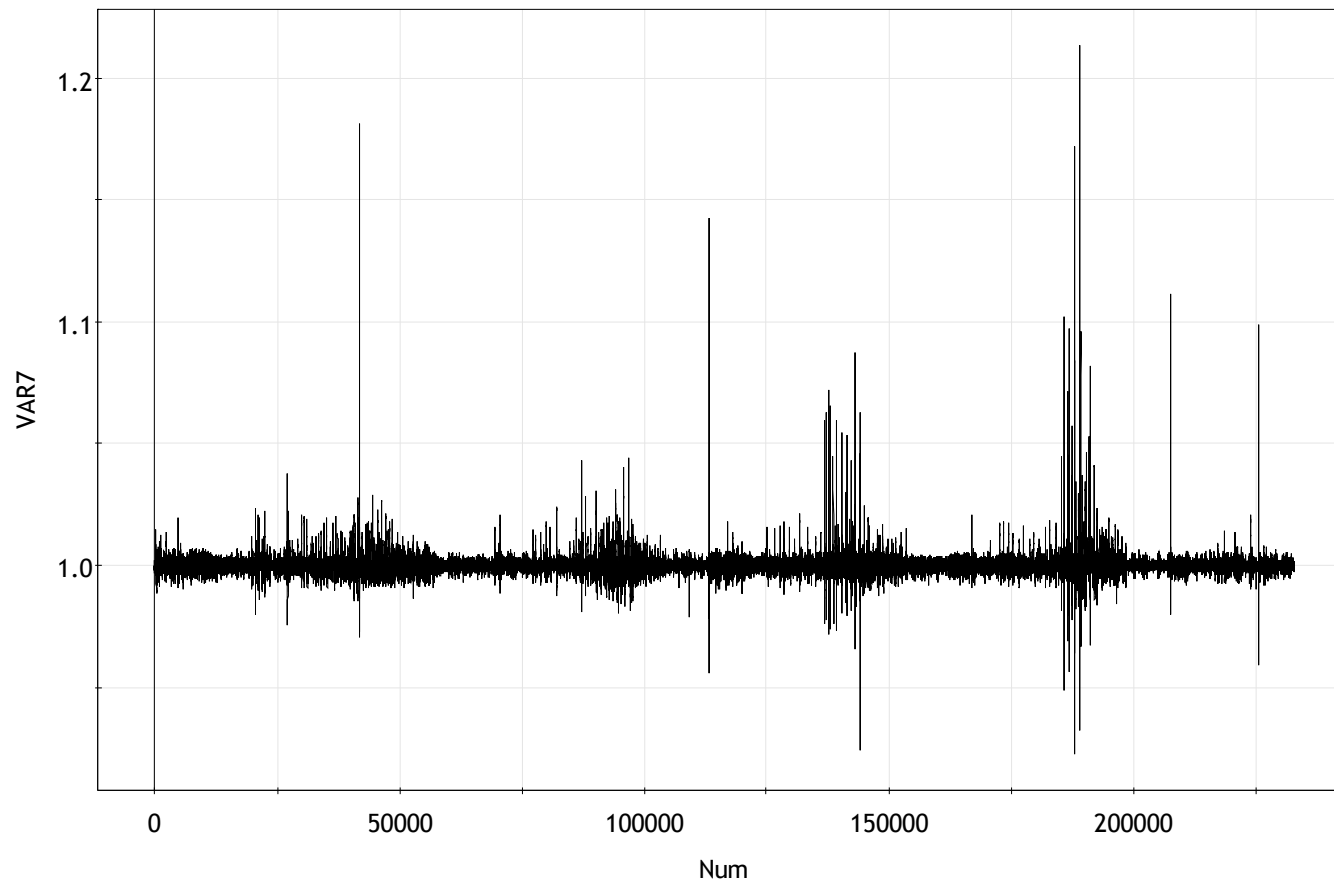
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- **Use risk assessment techniques prior to event if possible**
 - **Write regulatory filings carefully to avoid regulatory non compliance which would have no adverse patient affect**
 - **Example:**
 - A spray dryer indicates an outlet temperature of 123°C for 1 minute 17 seconds. The NDA/MAA filings state that the product is dried below 110°C. What do you do?
 - What temperature is the product?
 - Is primary drying over?
 - How long is the exposure?
 - What is the effect of the exposure?
 - Each particle is exposed for a very brief time – however long the excursion lasts.
 - When does a dryer ever show the actual product temperature?

Coping with perturbations

- Almost impossible to detect change once product enters CSTR stage
- Need to wait for equilibrium to be attained before the process change is possibly identifiable
- Use development data to confirm that the new conditions have the effect that you anticipate



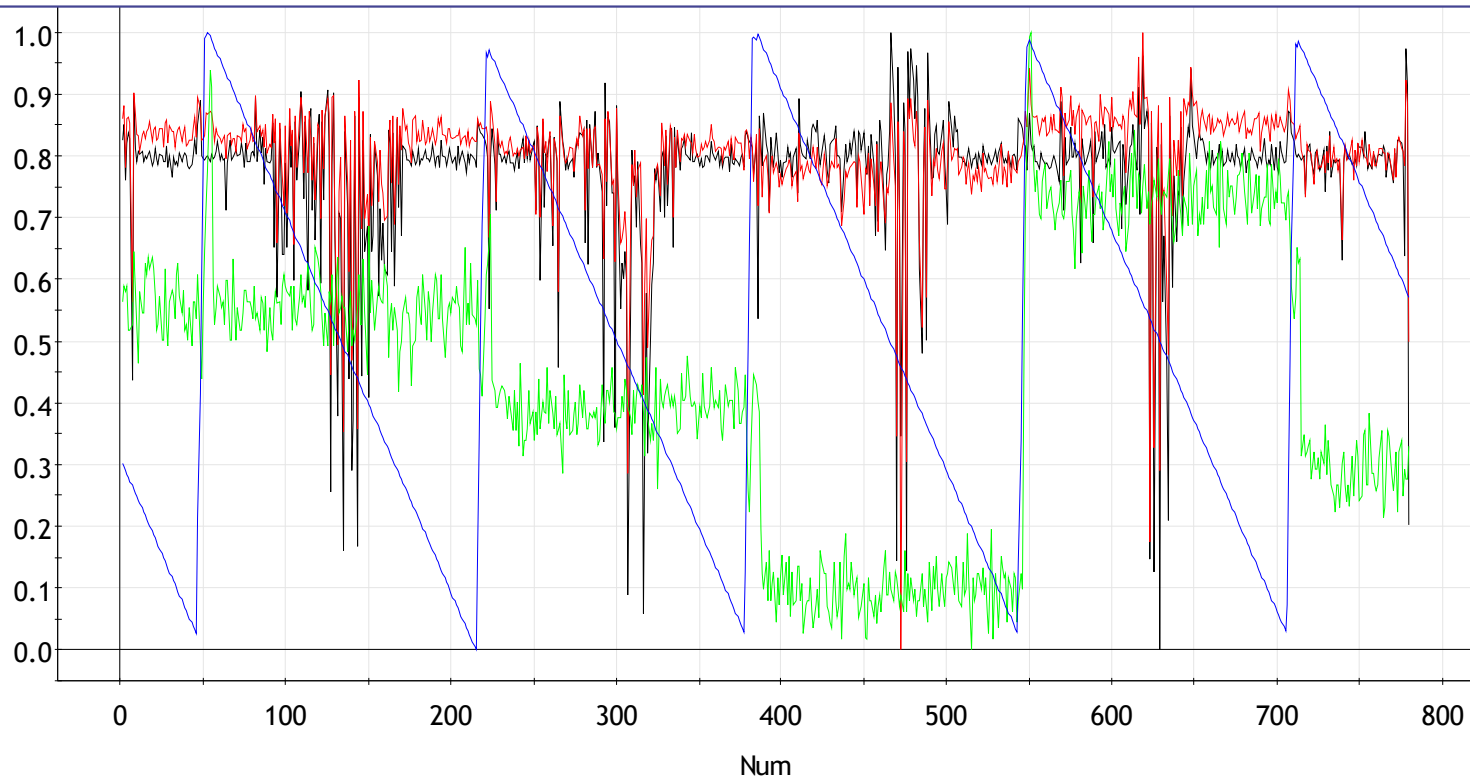
Example from commissioning (feed rate of a reactant with time) – raw data



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The explanation

Black = Feed rate reactant #1; Red = feed rate reactant #2; Green = Concentration (NIR) of reactant #1; Blue = fill level of vessel feeding reactant #1



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Regulatory impacts of continuous improvement

- **Write down your intention, not the way you have done it to date**
 - **A is added to B to give at least 80% C with no more than 2% D**

vs

- **Concentration X of A is added to concentration Y of B at Z litres/min maintaining the temperature between 5 and 10°C**
- **State criteria that you will use to implement improvement**
 - **Statistical methods, acceptance limits (not timelines) and how you will report them (Annual update, CBE0, etc.)**